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Thermal Dispersion Effects on Convection Heat Transfer in Porous Media with Viscous Dissipation

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ABSTRACT

The thermal dispersion effects on the Darcy–Forchheimer natural, mixed and forced convection heat transfer with viscous dissipation effects over an isothermal vertical flat plate in a fluid saturated porous media are examined numerically. The coefficient of thermal diffusivity has been assumed to be the sum of molecular diffusivity and the dispersion thermal diffusivity due to mechanical dispersion. The non-dimensional governing equations are solved by using finite difference method with a Crank Nicolson implicit numerical technique. The results show that in natural, mixed and forced convection heat transfer, when the modified Darcy number is increased the heat transfer rates are enhanced and when the modified Forchheimer number are increased the Nusselt numbers are decreased. The effect of both viscous dissipation and thermal dispersion was found to increase both velocities and temperatures inside boundary layer and to reduce heat transfer rates.

Keywords: Thermal dispersion, Viscous dissipation, Porous media, Convection heat transfer.

1. INTRODUCTION

The thermal dispersion effect on convection heat transfer through porous media was studied by many investigators for several cases with various procedures: analytically, numerically and experimentally. Significant advances have been made in modeling fluid flow, heat, and mass transfer through a porous medium including the Brinkman–Forchheimer-extended of Darcy law or the generalized model.

Representative studies in this area may be found in the recent research [1–4]. The magnetic field and heat generation effects were studied numerically by boundary layer analysis for free convection heat and mass transfer along a vertical plate for a nano-fluid saturated porous medium in the presence of viscous dissipation effect by Ram Reddy *et al.* [5]. The effects of variable viscosity and double dispersion on natural convection heat and mass transfer from a vertical cone in a saturated porous medium with non-Newtonian fluid was studied by Kairi [6]. The coupled heat and mass transfer by free convection in porous media had been presented for the case of vertical surface with linear temperature and concentration distribution by Rani and Rao [7]. Morth *at al.* [8] studied the case of horizontal surface with linear temperature and concentration distribution, a boundary layer analysis for the mixed convection from a

vertical plate embedded in a porous medium was presented. The effects of viscous dissipation on natural convection heat and mass transfer along a vertical plate embedded in saturated porous medium had been presented by MoorthY and Senthilvadivu [9]. The effect of variable viscosity on unsteady mixed convection boundary layer flow over a vertical surface embedded in a porous medium were obtained by Hassanien *et al.* [10]. The flow of an unsteady mixed-convection of fluid past an infinite vertical plate with time-dependent suction under the simultaneous effects of viscous dissipation was discussed by Ramreddy *et al.* [11]. Viscous dissipation effects on Darcy–Forchheimer mixed convection in a fluid saturated porous media were examined by Hamad and Bashir [12]. The MHD-mixed convection heat transfer problem was analyzed with viscous dissipation and Joule heating effects by Ibrahim *et al.* [13]. Convective flow and heat transfer in a square porous cavity was investigated numerically by Mahdy and Chamkha [14]. In this study, the thermal dispersion effects on the Darcy–Forchheimer natural, mixed and forced convection heat transfer with viscous dissipation effects over an isothermal vertical flat plate in a fluid saturated porous media will be examined numerically.

2. MATHEMATICAL FORMULATION

Attention will be concentrated on convection in a porous medium adjacent to a heated vertical flat plate, on which a thin thermal boundary layer is formed under the effect of externally forced and naturally heated stream flow over a vertical flat plate. As shown in following Figure the governing equations that describe the problem under consideration can be written as:

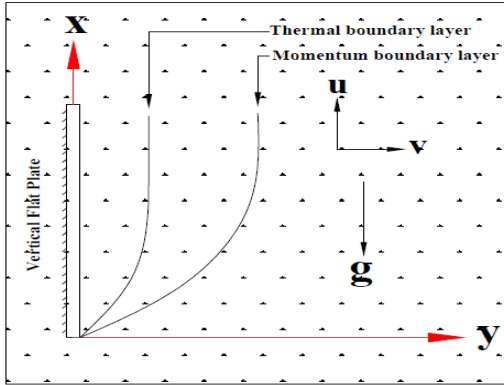


Figure 0. Geometry plate in saturated porous media

The continuity equation:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

The x-momentum equation:

$$\frac{\partial u}{\partial t} + \frac{\mu \varepsilon}{\rho K} u + \frac{C_F \varepsilon^2}{\sqrt{K}} u^2 = -\frac{1}{\rho} \frac{\partial P}{\partial x} + g_x \beta (T - T_\infty)$$

The y-momentum equation:

$$\frac{\partial v}{\partial t} + \frac{\mu \varepsilon}{\rho K} v + \frac{C_F \varepsilon^2}{\sqrt{K}} v^2 = -\frac{1}{\rho} \frac{\partial P}{\partial y} + g_y \beta (T - T_\infty)$$

The energy equation:

$$\begin{aligned} \frac{\partial T}{\partial t} + u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} \\ = \frac{k}{\rho C_p} \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right) \\ + \frac{v}{K C_p} u \left(u + \frac{C_F \sqrt{K}}{v} u^2 \right) \end{aligned}$$

With the following boundary conditions

$$\begin{aligned} y \rightarrow \infty \quad (v = 0, u = u_\infty \text{ \& } T = T_\infty) \\ y \rightarrow 0 \quad (v = 0 \text{ \& } T = T_w) \end{aligned}$$

Rewrite the y-momentum equation along the boundary layer edge ($y \rightarrow \infty$) utilizing the boundary conditions ($v = 0, u = u_\infty$ & $T = T_\infty$).

To find $\left[-\frac{1}{\rho} \frac{\partial P}{\partial x} \right]$. Then substitute it in the x-momentum equation to find the following equation.

$$\frac{\mu \varepsilon}{\rho K} (u_\infty - u) + \frac{C_F \varepsilon^2}{\sqrt{K}} (u_\infty^2 - u^2) + g_x \beta (T - T_\infty) = 0$$

The following dimensionless variables are defined:

$$\begin{aligned} X = \frac{x}{L}, Y = \frac{y}{L}, U = \frac{u}{u_\infty}, V = \frac{v}{u_\infty}, \theta = \frac{T - T_\infty}{T_w - T_\infty}, \\ \tau = \frac{U t}{L}, Gr = \frac{L g \beta (T_w - T_\infty)}{U_\infty^2}, Da^* = \frac{K \rho u_\infty}{\varepsilon L \mu}, \end{aligned}$$

$$Fr^* = \frac{\varepsilon^2 C_F L}{\sqrt{K}}, Pe = \frac{L u_\infty}{\alpha}, Ec = \frac{U_\infty^2}{C_p (T_w - T_\infty)}, T_d = \frac{\gamma d}{L}$$

where Da^* is the modified Darcy number, Fr^* is the modified Forchheimer number, Pe is Peclet Number, Ec is Eckert number and T_d is thermal dispersion number. So the continuity, the x-momentum and energy equations can be rewritten as:

$$\frac{\partial U}{\partial X} + \frac{\partial V}{\partial Y} = 0$$

- For natural convection heat transfer
-

$$U = \frac{-1}{2 Da^* Fr^*} + \left[\left(\frac{1}{2 Da^* Fr^*} \right)^2 + \frac{Gr \theta}{Fr^*} \right]^{\frac{1}{2}}$$

where u_∞ is reference velocity defined as:

$$u_\infty = -\frac{v}{2 \varepsilon C_F \sqrt{K}} + \left[\left(\frac{v}{2 \varepsilon C_F \sqrt{K}} \right)^2 + \frac{g \beta \sqrt{K} (T_w - T_\infty)}{\varepsilon C_F} \right]^{0.5}$$

- For mixed and forced convection heat transfer.

$$U = \frac{-1}{2 Da^* Fr^*} + \left[\left(\frac{1}{2 Da^* Fr^*} + 1 \right)^2 + \frac{Gr \theta}{Fr^*} \right]^{1/2}$$

Energy equation:

$$\begin{aligned} \frac{\partial \theta}{\partial \tau} + U \frac{\partial \theta}{\partial X} + V \frac{\partial \theta}{\partial Y} \\ = \left(\frac{1}{Pe} + T_d \right) \frac{\partial^2 \theta}{\partial Y^2} \\ + Ec U \left(\frac{1}{Da^*} U + Fr^* U^2 \right) \end{aligned}$$

The effective thermal diffusivity (α_e) may be expressed as $\alpha_e = \alpha + \alpha_d$. The molecular thermal diffusivity is assumed be constant and the dispersion thermal diffusivity is written as $\alpha_d = \gamma d u$.

3. NUMERICAL SOLUTION

Crank Nicolson implicit numerical technique will be used to solve the continuity, momentum and energy coupled equations. The dimensionless temperature and velocity derivative respect to x, y and τ will be written as:

The continuity equation:

$$V_{i,j}^{n+1} = -\frac{\Delta y}{\Delta x} [U_{i,j}^{n+1} - U_{i,j}^n] + V_{i-1,j}^{n+1}$$

The momentum Equation in x-direction:

$$U_{i,j}^{n+1} = \frac{-1}{2 Da^* Fr^*} + \left[\left(\frac{1}{2 Da^* Fr^*} + 1 \right)^2 + \frac{Gr \theta_{j,i}^{n+1}}{Fr^*} \right]^{0.5}$$

The Energy Equation:

$$\begin{aligned} \frac{\theta_{j,i}^{n+1} - \theta_{j,i}^n}{\Delta \tau} = & -U_{i,j}^n \left[\frac{\theta_{j,i+1}^n - \theta_{j,i}^n}{\Delta x} \right] \\ - & + \frac{V_{i,j}^n}{2} \left[\frac{\theta_{j+1,i}^{n+1} - \theta_{j,i}^{n+1} + \theta_{j+1,i}^n - \theta_{j,i}^n}{\Delta y} \right] \\ & + \left(\frac{1}{2 Pe} + \frac{T_d U_{j,i}^n}{2} \right) \dots \\ & \left[\frac{\theta_{j+1,i}^{n+1} - 2\theta_{j,i}^{n+1} + \theta_{j+1,i}^{n+1} + \theta_{j+1,i}^n - 2\theta_{j,i}^n + \theta_{j+1,i}^n}{(\Delta y)^2} \right] \\ & + Ec U_{j,i}^n \left[\frac{1}{Da^*} U_{j,i}^n + Da^* Fr^* (U_{j,i} \cdot U_{j,i})^n \right] \end{aligned}$$

After substituting the finite difference approximation in energy equation, it has the following form which includes three unknown at present time:

$$A_j \theta_{j+1,i}^{n+1} + B_j \theta_{j,i}^{n+1} + C_j \theta_{j-1,i}^{n+1} = D_j$$

$$A_j = 1 - \frac{V_{j,i}^n \Delta \tau}{2 (\Delta y)} + \frac{\Delta \tau}{Pe (\Delta y)^2} + \frac{T_d U_{j,i}^n \Delta \tau}{(\Delta y)^2}$$

$$B_j = \frac{V_{j,i}^n \Delta \tau}{2 (\Delta y)} + \frac{\Delta \tau}{2 Pe (\Delta y)^2} + \frac{T_d U_{j,i}^n \Delta \tau}{2 (\Delta y)^2}$$

$$C_j = -\frac{\Delta \tau}{2 Pe (\Delta y)^2} - \frac{T_d U_{j,i}^n \Delta \tau}{2 (\Delta y)^2}$$

$$\begin{aligned} D_j = & \theta_{i,j}^n + \Delta \tau \left[-U_{i,j}^n \frac{\theta_{j,i}^n - \theta_{j,i-1}^n}{\Delta x} \right. \\ & \left. - \frac{V_{i,j}^n}{2} \frac{\theta_{j+1,i}^n - \theta_{j,i}^n}{\Delta y} \right] \\ & + \left(\frac{1}{2 Pe} + \frac{T_d U_{j,i}^n}{2} \right) \left[\frac{\theta_{j+1,i}^n - 2\theta_{j,i}^n + \theta_{j-1,i}^n}{(\Delta y)^2} \right] \\ & + Ec U_{j,i}^n \left[\frac{1}{Da^*} U_{j,i}^n + Fr^* (U_{j,i} \cdot U_{j,i})^n \right] \end{aligned}$$

The boundary condition defined the dimensionless temperature at $y=0$ and $y=\infty$ are equal 1 and 0 respectively. At every i -line j will be equal 1, 2, 3... $n-1$, n . a set of n equations in the n unknown value of θ is obtained.

The above equation are solved to find the dimensionless temperature at certain i -line after that the dimensionless temperature will be founded at next i -line until all them will be calculated at every i and j at certain time until reaching steady state.

The local Nusselt number is given by:

$$Nu = \left[\frac{\theta_{j,i}^n - \theta_{j-1,i}^n}{\Delta y} \right]_{y=0}$$

4. RESULTS AND CONCLUSION

The velocity, temperature and local Nusselt number have been computed by using finite difference method (Crank Nicolson Technique). The numerical calculations are carried out for the effect of the modified Darcy number, modified Forchheimer number, viscous dissipation and thermal dispersion.

The velocity and temperature profiles and local Nusselt numbers for different values of modified Darcy number [1, 10, 100] and $Fr^*=0.1$, $Pe=7$, $Ec=0.01$, $T_d=0.1$, $Gr=1$ for natural, mixed and forced convection are drawn in Figures (1, 2, 3) respectively. It is clear that the increasing of modified Darcy number increased velocities and decreased thermal boundary layer thickness which results in higher coefficients of heat transfer. The effect of Forcheimer's number [0.05, 0.1, 0.5] and $Da^*=10$, $Pe=7$, $Ec=0.01$, $T_d=0.1$, on natural, mixed and forced convection are drawn if Figures (4, 5, 6). It is found that the increasing of Forecheimr's number decreased velocities and broadens temperature distribution and consequently decreased coefficient of heat transfer and Nusselt numbers.

The viscous dissipation effects are presented in Figures (7, 8, 9) for $Ec=0, 0.1, 0.2$ and $Da^*=10$, $Fr=0.1$, $Pe=7$, $T_d=0.1$, $Gr=1$. It is found that the increasing of viscous dissipation parameter or Eckert number had increased velocities inside boundary layers and heated the fluid which consequently decreased heat transfer rates; this is due to the important role played by viscosity in raising temperatures of flowing fluids.

The effects of thermal dispersion are shown if Figures (11, 12, 13) for different values of $T_d=0, 0.1, 0.2, 1$ and $Da^*=0.1$, $Fr^*=0.1$, $Pe=7$, $Ec=0.01$. It is clear that the effect of thermal dispersion is to increase both velocities and temperatures which consequently results in smaller heat transfer rates.

5. CONCLUSION

The thermal dispersion effects on the Darcy–Forchheimer natural, mixed and forced convection heat transfer with viscous dissipation effects over an isothermal vertical flat plate in a fluid saturated porous media are examined numerically. The non-dimensionalized conservation equations have been solved using the finite difference method whereas the coefficient of thermal diffusivity has been assumed to be the sum of molecular diffusivity and the dispersion thermal diffusivity due to mechanical dispersion. The major findings of the study are summarized as follows:

1. When the modified Darcy number is increased, the velocities inside boundary layers are increased and the temperatures are decreased which results in higher coefficients of heat transfer.

2. When the modified Forcheimer numbers are increased, the velocities are decreased and the temperatures are increased which decreased local Nusselt numbers.

3. When the Eckert numbers or viscous dissipation parameter are increased, both the velocities and temperatures are increased but the coefficients of heat transfer are decreased

4. When the thermal dispersion parameter is increased, both the velocities and temperatures are increased and local

• **Modified Darcy Number**

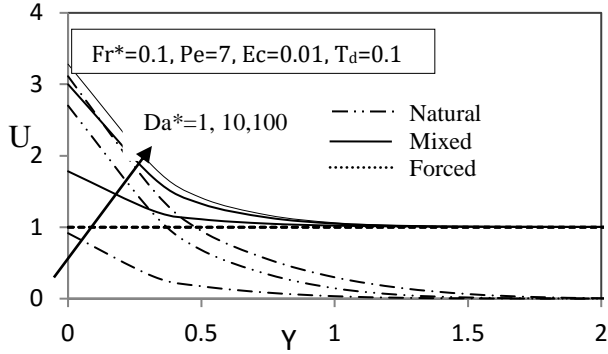


Figure 1. Dimensionless velocity Profiles for different values of modified Darcy number

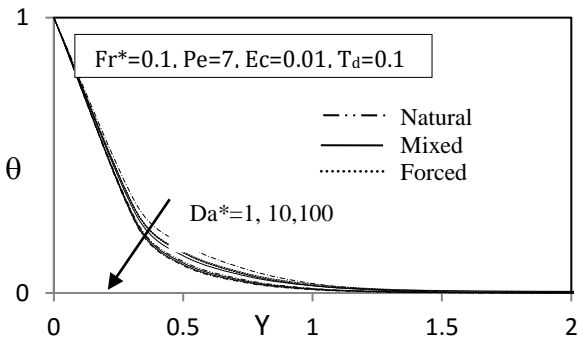


Figure 2. Dimensionless temperature Profiles for different values of modified Darcy number

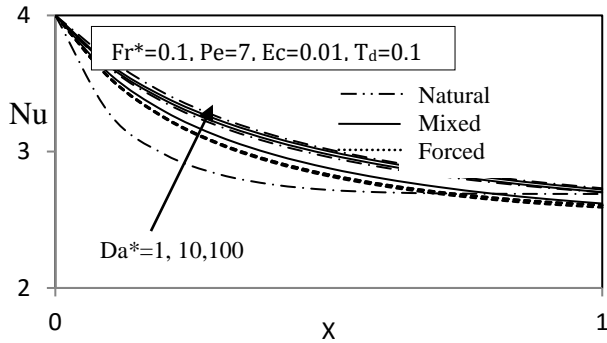


Figure 3. Local Nusselt number as function for different values of modified Darcy number

• **Modified Forchhimer Number**

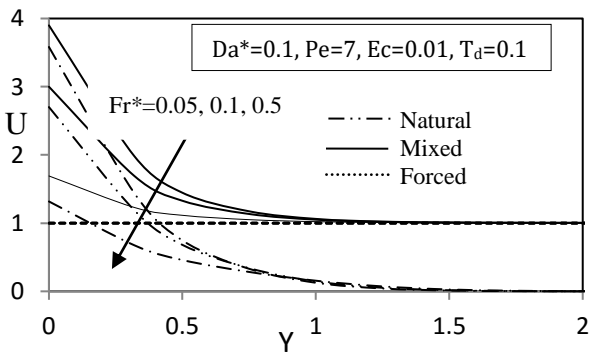


Figure 4. Dimensionless velocity Profiles for different values of modified Forchhimer number

Nusselt numbers are decreased; this is due to excessive heating of fluid layers.

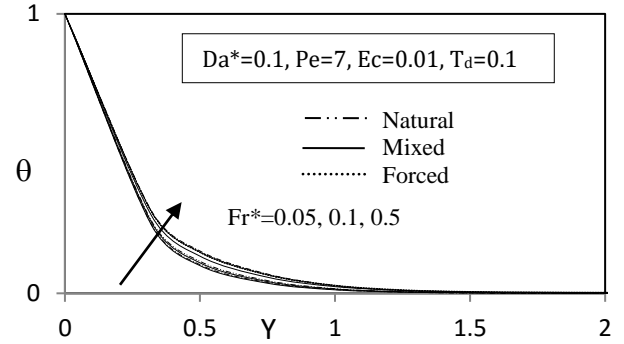


Figure 5. Dimensionless temperature Profiles for different values of modified Forchhimer number

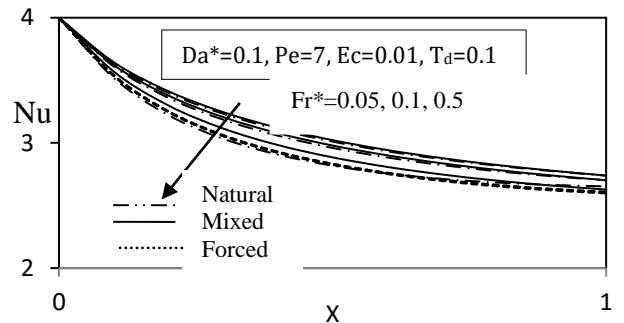


Figure 6. Local Nusselt number for different modified values of Forchhimer number

• **Viscous dissipation**

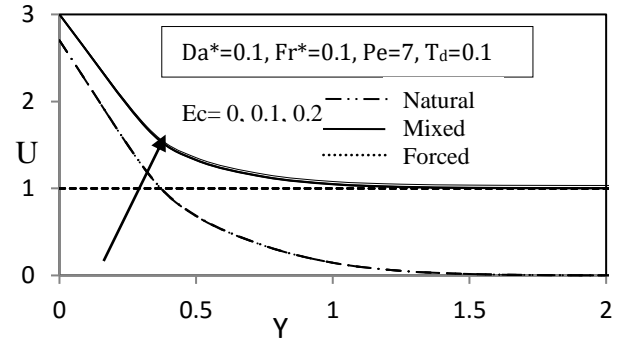


Figure 7. Dimensionless velocity Profiles for different values of viscous dissipation parameter

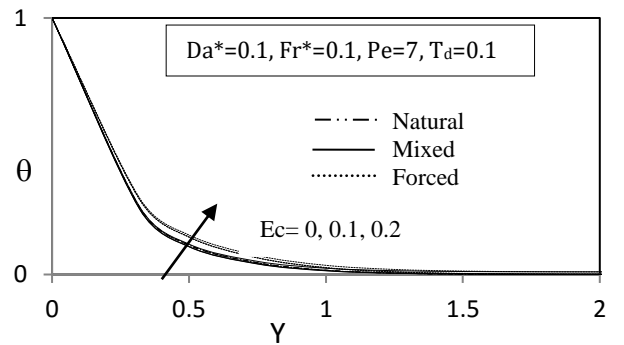


Figure 8. Dimensionless temperature Profiles for different values of viscous dissipation parameter

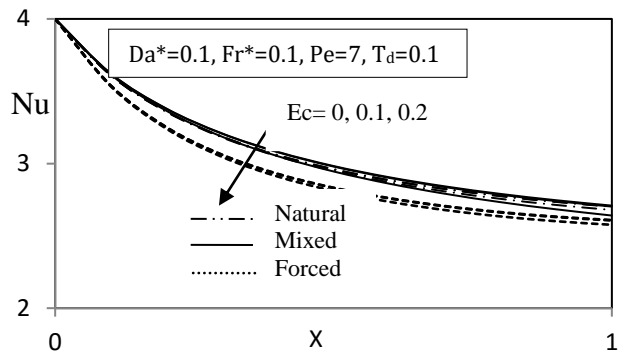


Figure 9. Local Nusselt number for different viscous dissipation

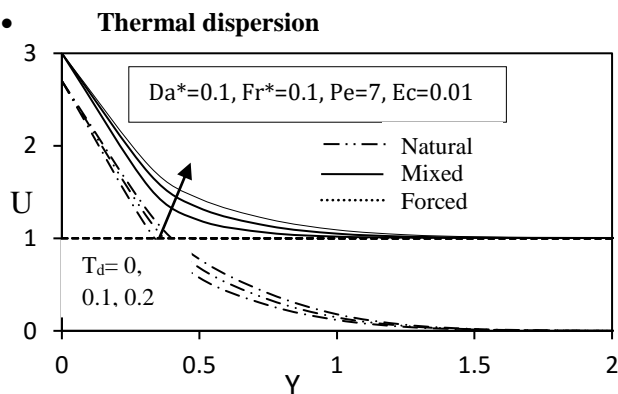


Figure 10. Dimensionless velocity Profiles for different values of thermal dispersion parameter

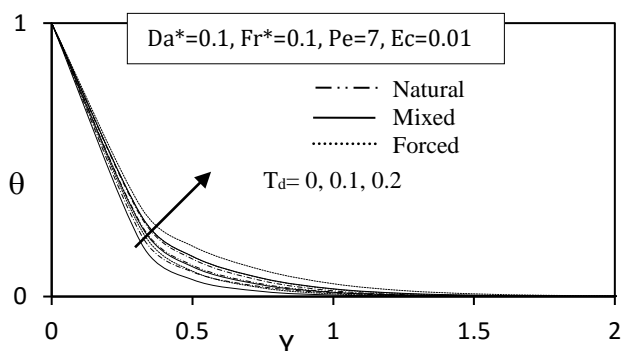


Figure 11. Dimensionless temperature Profiles for different values of thermal dispersion parameter

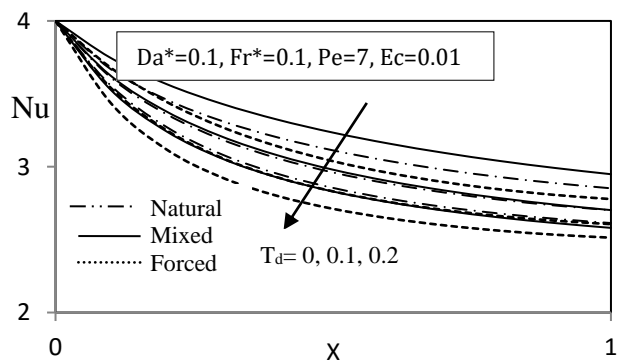


Figure 12. Local Nusselt number for different values of thermal dispersion parameter

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NOMENCLATURE

C_p	Specific heat (J/Kg.K).
C_f	Friction Coefficient.
g	Gravitational acceleration (m/s^2).
h	Convection heat transfer coefficient. ($W/m^2.k$).
K	Permeability (m^2).
Nu	Local Nusselt number.
q'	Heat transfer rate per unit length (W/m).
ε	The porosity of the porous medium.
u, v	Velocity components in x and y directions.
U, V	Dimensionless velocity components in x and y directions.

T	Temperature (K).
θ	Dimensionless temperature.
P	Pressure (Pa).
x	Axial coordinate along the plate (m).
X	Dimensionless axial coordinate along the plate.
y	Normal coordinate normal to the plate (m).
L	Length of vertical plate (m).
Y	Dimensionless vertical coordinate to the plate.
t	Time (s).
τ	Dimensionless time.
Gr	Grashof Number.
Da^*	Modified Darcy Number.
Fr^*	Modified Forchheimer Number.
Pe	Peclet number.
Ec	Eckert Number.
T_d	Thermal Dispersion Effect Number.

Greek letters

α_m	Effective thermal diffusivity of the porous media
α	Molecular thermal diffusivity.
α_d	Dispersion thermal diffusivity.
γ	Coefficient of mechanical dispersion.
d	Pore diameter.
μ	Dynamic viscosity
ν	Kinematic viscosity